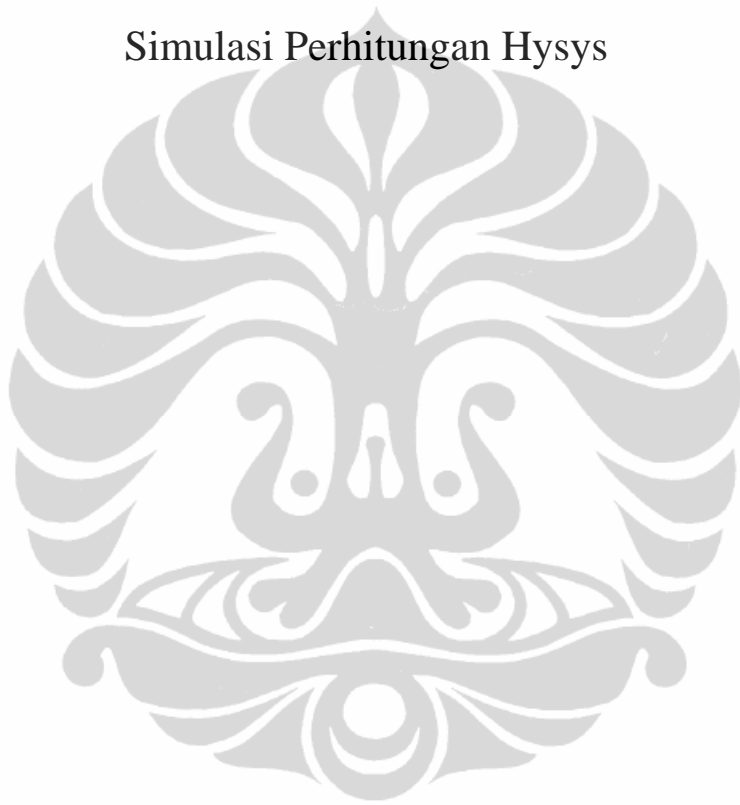


LAMPIRAN

Simulasi Perhitungan Hysys



Laju Alir LNG = 9125 m3/hari

Laju Alr Steam = 2700 m3/hari

Environment: Case (Main)
Mode: Steady State

Name	LNG in	LNG out	Steam in	Steam out
Vapour	0.0000	1.0000	0.0000	0.0000
Temperature [C]	-160.0	22.67	225.0	25.00
Pressure [bar]	20.00	19.95	34.47	34.42
Molar Flow [kgmole/h]	6725	6725	6245	6245
Mass Flow [tonne/d]	2892	2892	2700	2700
Std Ideal Liq Vol Flow [m3/d]	9125	9125	2705	2705
Molar Enthalpy [kJ/kgmole]	-9.250e+004	-7.731e+004	-2.690e+005	-2.853e+005
Molar Entropy [kJ/kgmole-C]	76.11	160.3	95.36	53.66
Heat Flow [kJ/h]	-6.220e+008	-5.199e+008	-1.680e+009	-1.782e+009

Laju Alir LNG = 18250 m3/hari

Laju Alr Steam = 5100 m3/hari

Environment: Case (Main)
Mode: Steady State

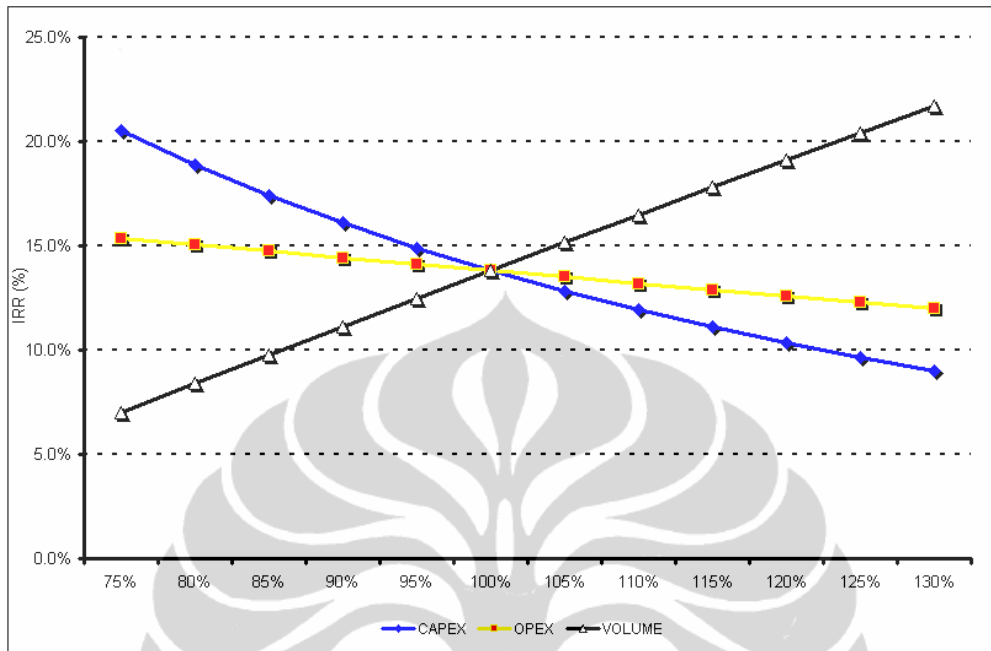
Name	LNG in	LNG out	Steam in	Steam out
Vapour	0.0000	1.0000	0.0000	0.0000
Temperature [C]	-160.0	5.413	225.0	25.00
Pressure [bar]	20.00	19.95	34.47	34.42
Molar Flow [kgmole/h]	1.345e+004	1.345e+004	1.191e+004	1.191e+004
Mass Flow [tonne/d]	5785	5785	5150	5150
Std Ideal Liq Vol Flow [m3/d]	1.825e+004	1.825e+004	5160	5160
Molar Enthalpy [kJ/kgmole]	-9.250e+004	-7.801e+004	-2.690e+005	-2.853e+005
Molar Entropy [kJ/kgmole-C]	76.11	157.9	95.36	53.66
Heat Flow [kJ/h]	-1.244e+009	-1.049e+009	-3.204e+009	-3.399e+009

LAMPIRAN

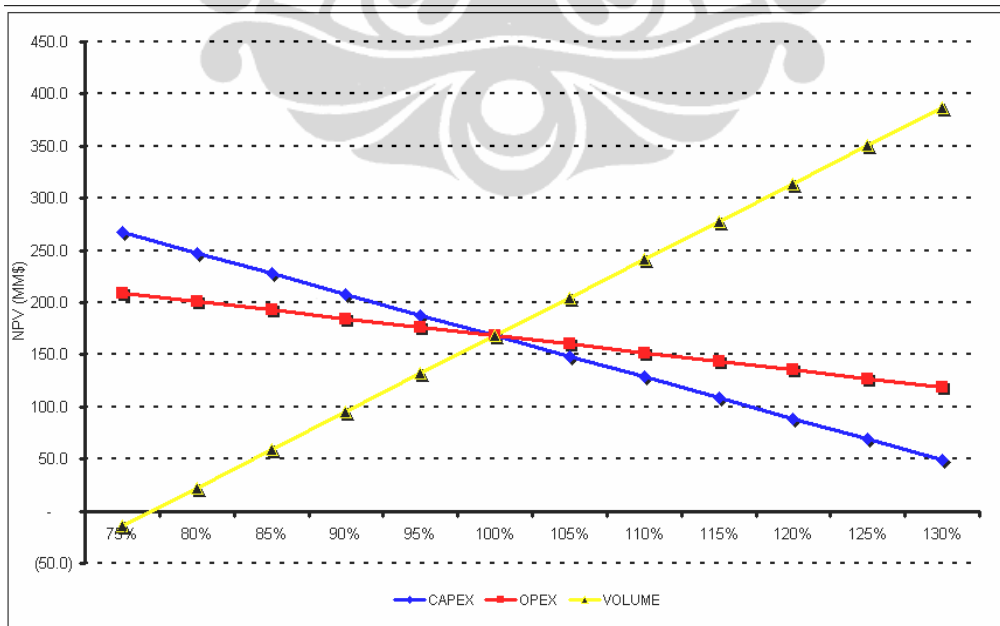
Simulasi Perhitungan Keekonomian



Sensitivitas IRR (IRROE 13.82%)

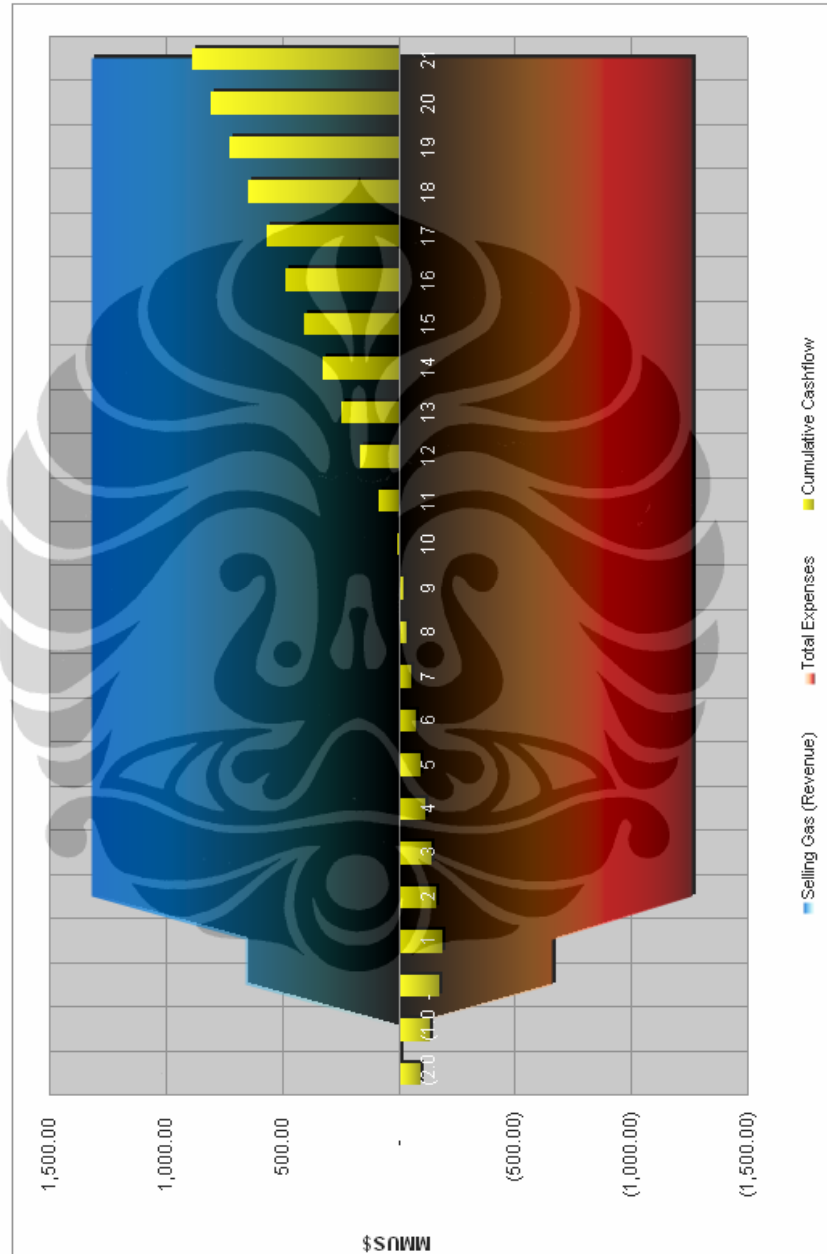


Sensitivitas NPV (IRROE 13.82%)



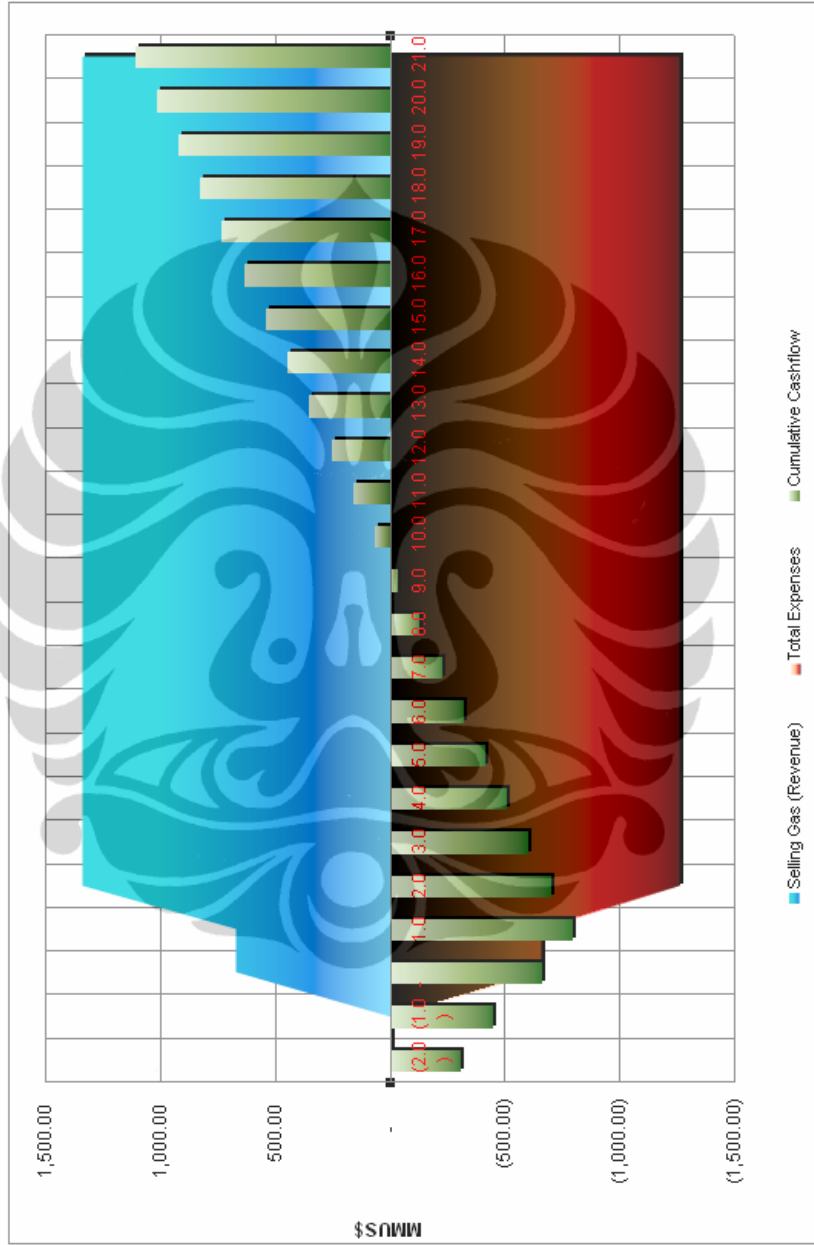
Cash Flow Profile

IRR/OE 13.82%



Cash Flow Profile

IRROI 8,26%



Cash Flow Calculation

IRROE 13.82%

Deskripsi	Scenario	Total	(2)	(1)	1	2	3	4	5	6	7	8	9	10
CAPEX		888,60 MM\$	306,2	138,6	261,6	-	-	-	-	-	-	-	-	-
- Train 1														
- LMG Receiving Terminal Construction Cost			306,2	138,6	261,6									
- Pre-operation Cost														
- Initial Working Capital														
- Train 2														
- LMG Receiving Terminal Construction Cost														
- Pre-operation Cost														
- Initial Working Capital														
- Land Acquisition Cost			10											
Production														
- Train 1	76.650,0 mmsed	1.638.300,0 mmsed			76.650,0	76.650,0	76.650,0	76.650,0	76.650,0	76.650,0	76.650,0	76.650,0	76.650,0	76.650,0
- Train 2	76.650,0 mmsed	1.533.000,0 mmsed			76.650,0	76.650,0	76.650,0	76.650,0	76.650,0	76.650,0	76.650,0	76.650,0	76.650,0	76.650,0
Total					153.300,000,0	153.300,000,0	153.300,000,0	153.300,000,0	153.300,000,0	153.300,000,0	153.300,000,0	153.300,000,0	153.300,000,0	153.300,000,0
Price														
- Selling Gas (Revenue)	8,53 \$/mmbtu	27.658,64 MM\$			658,5	1.317,1	1.317,1	1.317,1	1.317,1	1.317,1	1.317,1	1.317,1	1.317,1	1.317,1
- Buying Gas	1,53 \$/mmbtu	24.625,29 MM\$			516,8	1.033,6	1.033,6	1.033,6	1.033,6	1.033,6	1.033,6	1.033,6	1.033,6	1.033,6
DPEX	-335,543,320,000,00 \$/mmbtu													
Operational Cost					20,2	26,6	26,6	26,6	26,6	26,6	26,6	26,6	26,6	26,6
- Government Contribution					19,8	39,3	39,3	39,3	39,3	39,3	39,3	39,3	39,3	39,3
Depreciation		25.627,97 MM\$			616,7	1.233,7	1.233,7	1.233,7	1.233,7	1.233,7	1.233,7	1.233,7	1.233,7	1.233,7
Total Expense		26.516,57 MM\$			657,1	1.260,1	1.260,1	1.260,1	1.260,1	1.260,1	1.260,1	1.260,1	1.260,1	1.260,1
Cash Flow														
- Net Opr. Income		361,43 MM\$			1,4	24,2	26,8	23,6	32,7	36,0	33,6	43,4	47,6	52,1
- Tax	30%	288,43 MM\$			0,4	7,3	8,0	8,3	9,9	10,8	11,9	13,0	14,3	15,6
- NPV (Net Income After Tax)		85,16 MM\$	214,0	91,0	194,1	19,9	16,1	11,5	16,3	19,3	20,3	21,1	22,3	24,3
Share Value														
- NPV + Degr.		1773,72 MM\$	214,3	91,0	224,5	24,5	23,7	22,8	21,3	20,9	19,3	18,7	17,5	16,1
Cash Flow		885,12 MM\$	(31,3)	(41,6)	(31,3)	24,5	23,7	22,8	21,3	20,9	19,3	18,7	17,5	16,1
Cumulative Cashflow			(31,3)	(133,4)	(103,3)	(53,4)	(133,7)	(112,0)	(30,3)	(63,9)	(50,1)	(31,4)	(13,9)	2,2
REGAS FEE	1,07 \$/mmbtu													1,0
POT (PBP)	3,37 year													10,0
IRR	13,82%													
NPV	168,30 MM\$													
PI (BGR)	1,2													
Gas Sold Prices	8,53 \$/mmbtu													

Cash Flow Calculation

IRROE 13.82%

Deskripsi	Scenario	11	12	13	14	15	16	17	18	19	20
CAPEX											
- Train 1											
- LNG Receiving Terminal Construction Cost											
- Pre-operation Cost											
- Initial Working Capital											
- Train 2											
- LNG Receiving Terminal Construction Cost											
- Pre-operation Cost											
- Initial Working Capital											
- Land Acquisition Cost											
Production											
- Train 1	76.650.0 mmscf	76.650.0	76.650.0	76.650.0	76.650.0	76.650.0	76.650.0	76.650.0	76.650.0	76.650.0	76.650.0
- Train 2	76.650.0 mmscf	76.650.0	76.650.0	76.650.0	76.650.0	76.650.0	76.650.0	76.650.0	76.650.0	76.650.0	76.650.0
Total		153.300.000.0	153.300.000.0	153.300.000.0	153.300.000.0	153.300.000.0	153.300.000.0	153.300.000.0	153.300.000.0	153.300.000.0	153.300.000.0
Price											
- Selling Gas (Revenue)	8.59 \$/mmbtu	1,317.1	1,317.1	1,317.1	1,317.1	1,317.1	1,317.1	1,317.1	1,317.1	1,317.1	1,317.1
- Buying Gas	7.53 \$/mmbtu	1,153.6	1,153.6	1,153.6	1,153.6	1,153.6	1,153.6	1,153.6	1,153.6	1,153.6	1,153.6
OPEX	-335,543,320,000.00 \$/mmbtu										
- Operational Cost		26.6	26.6	26.6	26.6	26.6	26.6	26.6	26.6	26.6	26.6
- Government Contribution		39.5	39.5	39.5	39.5	39.5	39.5	39.5	39.5	39.5	39.5
OPEX		1,219.7	1,219.7	1,219.7	1,219.7	1,219.7	1,219.7	1,219.7	1,219.7	1,219.7	1,219.7
- Depreciation		40.4	40.4	40.4	40.4	40.4	40.4	40.4	40.4	40.4	40.4
Total Expense		1,260.1	1,260.1	1,260.1	1,260.1	1,260.1	1,260.1	1,260.1	1,260.1	1,260.1	1,260.1
Cash Flow											
- Net Opr. Income		57.0	57.0	57.0	57.0	57.0	57.0	57.0	57.0	57.0	57.0
- Tax	30%	17.1	17.1	17.1	17.1	17.1	17.1	17.1	17.1	17.1	17.1
NIAT (Net Income After Tax)		39.9	39.9	39.9	39.9	39.9	39.9	39.9	39.9	39.9	39.9
- Salvage value											
NIAT + Degr.		80.3	80.3	80.3	80.3	80.3	80.3	80.3	80.3	80.3	80.3
- Cash Flow		80.3	80.3	80.3	80.3	80.3	80.3	80.3	80.3	80.3	80.3
Cumulative Cashflow		82.5	162.7	243.0	323.3	403.5	483.8	564.1	644.3	724.6	804.9
REGAS FEE	107 \$/mmbtu	2.0	3.0	4.0	5.0	6.0	7.0	8.0	9.0	10.0	11.0
POT (PBP)	3.37 year										